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INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

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| Applicant's or agent's file reference BPCL 9944 | FOR FURTHER ACTION See Notification of Transmittal of International Preliminary Examination Report (Form PCT/IPEA/416) | | | | |
| International application No. PCT/GB 03/04052 | International filing date (day/mont/ 23.09.2003 | hlyear) Priority date (day/monthlyear) 08.10.2002 | | | |
| International Patent Classification (IPC) or be | oth national classification and IPC | | | | |
| C10G70/02 | | | | | |
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| Applicant | | | | | |
| BP CHEMICALS LIMITED et al | | | | | |
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| This international preliminary examples to the Authority and is transmitted to the Authority and is transmitted to the Authority and is transmitted. | This International preliminary examination report has been prepared by this International Preliminary Examining Authority and is transmitted to the applicant according to Article 36. | | | | |
| Authority and is numerimize to the | applicant according to Article of | o. | | | |
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| 2. This REPORT consists of a total of | of 5 sheets, including this cover | sheet. | | | |
| ☐ This report is also accompa | nied hy ANNEXES, i.e. sheets of | f the description, claims and/or drawings which have | | | |
| been amended and are the | basis for this report and/or sheet | s containing rectifications made before this Authority | | | |
| (See Hule 70.16 and Section | n 607 of the Administrative Instru | uctions under the PCT). | | | |
| These annexes consist of a total of | of 3 sheets. | • | | | |
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| 3 This report contains indications re | alating to the following items: | | | | |
| 3. This report contains indications re | elating to the following items: | • | | | |
| l ⊠ Basis of the opinion | elating to the following items: | • | | | |
| I 🖾 Basis of the opinion | | | | | |
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INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No.

PCT/GB 03/04052

| i. | Bas | is | of | the | rep | ort |
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1. With regard to the **elements** of the international application (Replacement sheets which have been furnished to the receiving Office in response to an invitation under Article 14 are referred to in this report as "originally filed" and are not annexed to this report since they do not contain amendments (Rules 70.16 and 70.17)):

| | Des | cription, Pages | | | | |
|---|--|--|--|-------------------------------------|--|--|
| | 1-23 | 3 | as originally filed | | | |
| | Clai | ms, Numbers | the many and the same and the s | . Post of | | |
| | 1-16 | 3 | received on 22.12.2004 with letter of 21.12.2004 | | | |
| 2. | With lang | regard to the langu a uage in which the inte | age, all the elements marked above were available or furnished ternational application was filed, unless otherwise indicated under | o this Authority in the rthis item. | | |
| | The | se elements were ava | ailable or furnished to this Authority in the following language: | , which is: | | |
| | | the language of publi | nslation furnished for the purposes of the international search (uication of the international application (under Rule 48.3(b)). Inslation furnished for the purposes of international preliminary expenses. | · | | |
| Rule 55.2 and/or 55.3). With regard to any nucleotide and/or amino acid sequence disclosed in the international application, the international preliminary examination was carried out on the basis of the sequence listing: | | | | | | |
| | | contained in the inter | rnational application in written form. | | | |
| | . 🗆 | filed together with the | e international application in computer readable form. | +3 *v | | |
| | | furnished subsequen | itly to this Authority in written form. | | | |
| | | furnished subsequen | tly to this Authority in computer readable form. | | | |
| | ☐ The statement that the subsequently furnished written sequence listing does not go beyond the disclosure in the international application as filed has been furnished. | | | | | |
| | | The statement that the listing has been furni | ne information recorded in computer readable form is identical to shed. | the written sequence | | |
| 4. | The | amendments have re | esulted in the cancellation of: | | | |
| | | the description," | pages: | 1.41% | | |
| | | the claims, | Nos.: | | | |
| | | the drawings, | sheets: | | | |
| 5. | | This report has been been considered to g | established as if (some of) the amendments had not been made go beyond the disclosure as filed (Rule 70.2(c)). | , since they have | | |
| | | (Any replacement sh report.) | neet containing such amendments must be referred to under item | 1 and annexed to this | | |
| 6. | Add | litional observations i | f necessary | | | |

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No.

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| ٧. | Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability |
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| | citations and explanations supporting such statement |

1. Statement

Novelty (N) Yes: Claims 1-16

No: Claims

Inventive step (IS) Yes: Claims 1-16

No: Claims

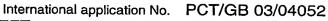
Industrial applicability (IA)... ... Yes:. Claims 1-16

No: Claims

2. Citations and explanations

see separate sheet

INTERNATIONAL PRELIMINARY



EXAMINATION REPORT - SEPARATE SHEET

Re Item V

Reasoned statement with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

Reference is made to the following document/s/:

D1: US-A- 4 299 800 D2: GB-A-565 991

The document D2 is regarded as being the closest prior art to the subject-matter of claims 1 and discloses (page 1, lines 58-98) a process for removing oxygen from oxygen containing gaseous olefines, which process comprises contacting the gas mixture with a catalyst. Metals or oxides of nickel, platinum and palladium are disclosed as preferred catalysts.

The subject-matter of claim 1 differs from this known D2 in that the catalyst also comprises tin.

The subject-matter of claim 1 is therefore new (Article 33(2) PCT).

The presence of tin in the catalyst improves the removal of oxygen. Thus the subjectmatter of claim 1 is also considered as involving an inventive step (Article 33(3) PCT.

The document D1 is regarded as being the closest prior art to the subject-matter of claims 2 and discloses (col 1, line 54- col 2, line 60);

a method for the removal of oxygen from a gas mixture comprising oxygen, olefin, hydrogen and carbon monoxide which process comprises contacting the gas mixture with a silver and/ or gold catalyst (metals of the 11 th group of the Periodic Table of Elements). Zeolite is explicitly disclosed as a possible catalyst support.

The subject-matter of claim 2 differs from this known D1 in that, in addition to oxygen. alkyne is also removed from the gas mixture.

The subject-matter of claim 2 is therefore new (Article 33(2) PCT).

When the gas mixture comprises alkyne in addition to olefin and oxygen the performance of copper (or silver or gold) in the process of removing oxygen and alkyne from a gas mixture can be improved by being supported on a zeolite. Thus the subjectmatter of claim 2 is also considered as involving an inventive step (Article 33(3) PCT.





INTERNATIONAL PRELIMINARY **EXAMINATION REPORT - SEPARATE SHEET**

International application No. PCT/GB 03/04052

Claims 3-16 are dependent on claim 1 or 2 and as such also meet the requirements of the PCT with respect to novelty and inventive step.



. Case 9944(2)

Claims

- 1. A process for the removal of oxygen from a gas mixture comprising oxygen, at least one olefin, hydrogen, carbon monoxide and optionally at least one alkyne, the ratio of oxygen: hydrogen in the gas mixture being 1 part by volume of oxygen to at least 5 parts by volume of hydrogen, which process comprises contacting the gas mixture with a catalyst in a reaction zone under conditions sufficient to oxidise at least a portion of the hydrogen and to oxidise at least a portion of the carbon monoxide and without significant hydrogenation of the at least one olefin, wherein the catalyst comprises at least one metal or oxide of a metal from the 10th group of the Periodic Table of Elements, the metal or oxide of the metal being supported on an oxide support, provided that the catalyst also comprises tin.
- 2. A process for the removal of oxygen and alkyne from a gas mixture comprising oxygen, at least one olefin, hydrogen, carbon monoxide and at least one alkyne, the ratio of oxygen: hydrogen in the gas mixture being at least 1 part by volume of oxygen to at least 5 parts by volume of hydrogen, which process comprises contacting the gas mixture with a catalyst in a reaction zone under conditions sufficient to oxidise at least a portion of the hydrogen and to oxidise at least a portion of the carbon monoxide and without significant hydrogenation of the at least one olefin, wherein the catalyst comprises at least one metal or oxide of a metal selected from the group consisting of the 10th group and the 11th group of the Periodic Table of Elements, the metal or oxide of the metal being supported on an oxide support, provided that where the catalyst comprises at least one metal or oxide of a metal from the 10th group of the Periodic Table of Elements supported on an oxide support, the catalyst also comprises tin and



provided that where the catalyst comprises at least one metal or oxide of a metal of the 11th group of the Periodic Table of Elements the oxide support is a zeolite.

- 3. A process according to claim 1 or claim 2 wherein the gas mixture contains 2000 ppm or less of oxygen.
- 4. A process according to any one of claims 1 to 3 wherein the gas mixture comprises at least 10 vol% of hydrogen.
- 5. A process according to claim 4 in which the gas mixture comprises at least 20 vol % hydrogen.
- 6 A process according to any one of the preceding claims in which the gas mixture comprises from greater than 0 up to and including 20 vol % alkyne.
- 7. A process according to claim 6 in which the alkyne is acetylene.
- 8. A process according to anyone of claims 2 to 7 wherein the catalyst comprises at least 0.01wt%, based on the total weight of the dry catalyst, of at least one metal or oxide of a metal selected from copper, silver and gold, supported on a zeolite support.
- 9. A process according to claim 8 in which the catalyst comprises copper in an amount in the range of from 1 to 15 wt %.
- 10. A process according to claim 8 or claim 9 wherein the zeolite is zeolite A or zeolite X.
- 11. A process according to any one of claims 1 to 7 in which the catalyst comprises at least 0.01 wt%, based on the total weight of the dry catalyst, of at least one metal or oxide of a metal selected from nickel, palladium and platinum supported on silica or alumina.
- 12. A process according to claim 11 wherein the metal is platinum and is present in an amount in the range 0.01 15 wt% based on the total weight of the dry catalyst and is supported on silica.
- 13. A process according to claim 11 or claim 12 wherein tin is present in the catalyst in an amount in the range 0.01 to 60 wt% based on the total dry weight of the catalyst.
- 14. A process according to any one of the preceding claims wherein the gas mixture is contacted with the catalyst in the reaction zone at a temperature in the range 50-300° C.
- 15. A process according to anyone of the preceding claims wherein the gas mixture is contacted with the catalyst in the reaction zone at a total pressure in the range 15-35 bara.



- 16. A process according to any one of the preceding claims wherein the process comprises the steps:
- (a) contacting at least one hydrocarbon with a molecular oxygen-containing gas in a first reaction zone with a catalyst capable of supporting combustion beyond the normal fuel-rich limit of flammability and wherein the stoichiometric ratio of hydrocarbon to oxygen is 5 to 16 times the stoichiometric ratio of hydrocarbon to molecular oxygen-containing gas for complete combustion to carbon dioxide and water, to produce a product stream comprising oxygen, at least one olefin, hydrogen, carbon monoxide and optionally at least one alkyne,
- (b) contacting in a second reaction zone, at least a portion of the product stream from step (a) having a ratio of oxygen to hydrogen of at least one part by volume of oxygen to at least 5 parts by volume of hydrogen with a catalyst under conditions sufficient to oxidise at least a portion of the hydrogen and to oxidise at least a portion of the carbon monoxide and without significant hydrogenation of the at least one olefin, wherein the catalyst comprises at least one metal or oxide of a metal selected from the group consisting of the 10th group and the 11th group of the Periodic Table of Elements, the metal oxide of the metal being supported on an oxide support, provided that where the catalyst comprises at least one metal or oxide of a metal from the 10th group of the Periodic Table of Elements supported on an oxide support, the catalyst also comprises tin and provided that where the catalyst comprises at least one metal or oxide of a metal of the 11th group of the Periodic Table of Elements the oxide support is a zeolite.